GWANDA STATE UNIVERSITY

# FACULTY OF ENGINEERING AND ENVIRONMENT <br> DEPARTMENT OF METALLURGICAL ENGINEERING <br> PARTICULATE SYSTEMS 

EMR 5201
Part V Second Semester Examination Paper
August 2022

This examination paper consists of 4 printed pages
Time Allowed: 3 hours
Total Marks: 100

## INSTRUCTIONS

1. Answer ALL questions in Section A and any TWO from Section B
2. Each question carries 25 marks
3. Use of calculators is permissible

## Additional Requirements

1. Calculator

## MARK ALLOCATION

| Section A | 50 Marks |
| :--- | :--- |
| Section B | 50 Marks |
| Part Questions | As shown in each part question |
| Total Attainable | 100 |

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EMR 5201 Particulate systems

## SECTION A (50 MARKS)

## ANSWER ALL QUESTIONS

## Question A1

a) With the aid of a diagram, explain how shape, size and composition of gold ore particles affect its recovery by froth flotation
b) Consider a cuboid particle having the following dimensions $5 \mathrm{~mm} \times 3 \mathrm{~mm} \times 1 \mathrm{~mm}$. Calculate the following diameters of the particle:
i.the volume diameter
ii. the surface diameter [3]
iii. the surface-volume diameter [4]
iv. the sieve diameter [3]
v. the projected area diameters [4]

## Question A2

a) Explain using a metallurgical process of choice, three factors to be considered when selecting a filtration process
b) Company X would like to generate energy using a fluidized bed chamber to combust coal fines. Considering the chief behaviour characteristics of the four Geldart powder groups, explain how the energy generation will be affected by the group in which the coal fines fit
c) A sphere of diameter 10 mm and density $7700 \mathrm{~kg} / \mathrm{m}^{3}$ falls under gravity at terminal conditions through a liquid of density of $900 \mathrm{~kg} / \mathrm{m}^{3}$ in a tube of diameter of 12 mm . The measured terminal velocity of the particle is $1.6 \mathrm{~mm} / \mathrm{s}$.
i. Calculate the viscosity of the fluid.
ii. Verify if stoke's law applies

## SECTION B (50 MARKS)

## ANSWER ANY TWO QUESTIONS

## Question B1

a) Distinguish between the cumulative and differential analysis of particles [4]
b) Outline and explain two forces that affect the motion of particles in a fluid
c) Approximately, 3.6 kg of solid particles of density $2590 \mathrm{~kg} / \mathrm{m}^{3}$ and surface-volume mean size 748 mm form a packed bed of height 0.475 m in a circular vessel of diameter 0.0757 m . Water of density $1000 \mathrm{~kg} / \mathrm{m}^{3}$ and viscosity 0.001 Pa s is passed upwards through the bed. Calculate
i. the bed pressure drop at incipient fluidization,
ii. the superficial liquid velocity at incipient fluidization,
iii. the mean bed voidage at a superficial liquid velocity of $1.0 \mathrm{~cm} / \mathrm{s}$,
iv. the bed height at this velocity and
v. the pressure drop across the bed at this velocity.

## Question B2

a) What are the advantages and disadvantages of wet and dry screening
b) Define sphericity and shape factor
c) The size distribution of a dust as measured by a microscope is as follows.
i. Convert the data below to obtain the distribution on a mass basis,
ii. Calculate the specific surface, assuming spherical particles of density $2650 \mathrm{~kg} / \mathrm{m}^{3}$ [7]

| Size range (um) | Number of particles in range |
| :---: | :---: |
| $0-2$ | 2000 |
| $2-4$ | 600 |
| $4-8$ | 140 |
| $8-12$ | 40 |
| $12-16$ | 15 |
| $16-20$ | 5 |
| $20-24$ | 2 |

## Question B3

a) With the aid of a diagram explain the fluidisation process
b) For high Reynolds number ( $>500$ ) flow of a fluid through a packed bed of particles how does the frictional pressure drop across the bed depend on
i. superficial fluid velocity,
ii. particle size,
iii. fluid density,
iv. fluid viscosity
v. voidage
c) A packed bed of solid particles of density $2500 \mathrm{~kg} / \mathrm{m}^{3}$ occupies a depth of 1 m in a vessel of cross-sectional area $0.04 \mathrm{~m}^{2}$. The mass of solids in the bed is 50 kg and the surface volume mean diameter of the particles is 1 mm . A liquid of density $800 \mathrm{~kg} / \mathrm{m}^{3}$ and viscosity 0:002 Pa s flows upwards through the bed, which is restrained at its upper surface.
i. Calculate the voidage (volume fraction occupied by voids) of the bed.
ii. Calculate the frictional pressure drop across the bed when the volume flow rate of liquid is $1.44 \mathrm{~m}^{3} / \mathrm{h}$.

## END OF QUESTION PAPER

